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# Concentration of carbon dioxide in the water-phase as a parameter to model the effect of a modified atmosphere on microorganisms

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## Abstract

The effect of modified atmosphere packaging can mainly be attributed to the bacteriostatic action of CO<sub>2</sub>. The dissolved CO<sub>2</sub> in the water-phase of a food product is strongly dependent on several intrinsic and extrinsic parameters and will determine the effectiveness of a modified atmosphere packaging configuration. The effect of pH, gas/product ratio, initial %CO<sub>2</sub> in the gas-phase, lard content and storage temperature on the amount of dissolved CO<sub>2</sub> was screened in a preliminary experiment. The initial CO<sub>2</sub>-concentration in the gas-phase and the gas/product ratio turned out to be the two major factors determining the amount of dissolved CO<sub>2</sub>. The initial pH also determined significantly the final CO<sub>2</sub>-concentration in the broth. Temperature and lard content were shown to have only a minor effect on the amount of dissolved CO<sub>2</sub> compared to the above mentioned parameters. This demonstrates the importance of the packaging configuration in the effectiveness of a modified atmosphere. In a second step, a model was constructed to predict the amount of dissolved carbon dioxide in modified BHI-broth as a function of the gas/product ratio, the initial CO<sub>2</sub>-concentration and the temperature by means of Response Surface Methodology (RSM). A second equation was also derived based on Henry's law and was shown to be a powerful tool in the quantification of the effect of intrinsic and extrinsic parameters on the CO<sub>2</sub>-solubility in food products. The possibility of the use of the concentration of dissolved CO<sub>2</sub> in the water-phase as a determinative factor for the inhibitory effect of modified atmospheres was examined on *Pseudomonas fluorescens*. Growth curves at 7°C of *P. fluorescens* in different packaging configurations (initial %CO<sub>2</sub> and gas/product ratio) resulting in equal amounts of dissolved CO<sub>2</sub> were compared. *P. fluorescens* was shown to be similarly inhibited by equal amounts of dissolved CO<sub>2</sub>-concentrations, independent of the packaging configuration. This demonstrates the potential of the application of the concentration of dissolved CO<sub>2</sub> in the water-phase as a parameter to characterise a modified atmosphere and its inhibition of certain microorganisms. © 1998 Elsevier Science B.V. All rights reserved.

**Keywords:** Modified atmosphere packaging; Carbon dioxide; Solubility; Water-phase

## 1. Introduction

Modified atmosphere packaging (MAP) has been shown to be very effective in extending the shelf-life

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of fresh and processed chilled products. Research regarding MAP has concentrated on the optimisation of gas mixtures for specific products (Zeitoun et al., 1994; Nissen et al., 1996; Jiménez et al., 1997; Boskou and Debevere, 1998) and on the safety of MAP-products (Berrang et al., 1989; Özbas et al., 1996; Beumer et al., 1996; Fernandez et al., 1997; Sutherland et al., 1997). In this type of study, the activity of CO<sub>2</sub> on the microbial growth has always been related to the initial concentration of CO<sub>2</sub> in the gas-phase of the package. Very often, the gas/product volume ratio is not mentioned which makes it very difficult to compare results.

CO<sub>2</sub> is because of its antimicrobial activity the most important component in the applied gas mixtures. When CO<sub>2</sub> is introduced into the package, it is partly dissolved in the water-phase and the fat-phase of the food. This results after equilibrium in a certain concentration of dissolved CO<sub>2</sub> in the water-phase of the product. Little work has been reported regarding the factors affecting the CO<sub>2</sub>-solubility in MAP products. Zhao et al. (1994) modeled the CO<sub>2</sub> solubilized in beef during time. Fava and Pergiovanni (1992) correlated the CO<sub>2</sub>-solubility in foods packed in modified atmospheres with some chemical-physical characteristics ( $a_w$ , pH) and composition of the food (moisture, fat and protein content). Löwenadler and Rönner (1994) demonstrated an important effect of the buffer capacity of the food and the ratio of head space to media volume on the solubility of CO<sub>2</sub>. Gill (1988) showed a significant effect of temperature, type of fat tissue and fat content on the solubility of CO<sub>2</sub> in meat. Lower solubility at higher temperatures has been mentioned by many authors (Wolfe, 1980; Wimpfheimer et al., 1990; Zhao et al., 1994) as the reason for the minor effect of MAP at higher temperatures.

In this paper the effect of intrinsic (pH, fat content) and extrinsic (temperature, gas/product volume ratio and initial CO<sub>2</sub>-concentration in the gas-phase) parameters on the amount of CO<sub>2</sub> which dissolves in the water-phase of a food when packed under modified atmospheres is quantified by means of a fractional factorial design screening experiment. Furthermore, a response surface model is developed for the amount of CO<sub>2</sub> which dissolves in broth, as a function of the temperature, the gas/product volume ratio and the initial CO<sub>2</sub>-concentration in the gas-

phase. In a third part the possibility to use the amount of dissolved CO<sub>2</sub> in the water-phase as a parameter for the effectiveness of a modified atmosphere is illustrated with *Pseudomonas fluorescens* as test organism.

## 2. Materials and methods

### 2.1. Screening for the importance of intrinsic and extrinsic factors on the CO<sub>2</sub>-solubility

#### 2.1.1. Sample preparation

Experiments were performed in 600-ml jars, specially constructed for this purpose, provided with a Teflon valve and a central opening which was closed with a silicone septum. The glass jars were filled with the appropriate amount of modified BHI (Brain Heart Infusion, Gibco BRL + 18 g/l glucose (Sigma, G8270), 3 g/l yeast extract (Oxoid, L21) and 20 g/l NaCl (Vel, 1723)) and autoclaved at 121°C for 15 min. The pH was adjusted after autoclaving to the appropriate value with sterile 2 N HCl or 2 N NaOH. To investigate the effect of the presence of fat on the CO<sub>2</sub>-solubility in the water-phase, a specific quantity of lard was added to the broth. The bottles were placed in an impermeable bag (Sidamil, UCB Transpac, Gent, Belgium; O<sub>2</sub>-permeability: 6 ml/m<sup>2</sup>/24 h, CO<sub>2</sub>-permeability: 2 ml/m<sup>2</sup>/24 h at 25°C, 100% R.H.), the valve opened and gas packed (gas mixer: WITT MG18-3MSO, Gasetechnik, Germany and gas packaging: MULTIVAC A300/42, Sepp. Hagenmüller KG, Wolfertschwenden, Germany) at the desired gas composition (gasses: Air Products, Vilvoorde, Belgium). The bottles were closed 30 s after packaging, removed from the bag and stored at the appropriate temperature  $\pm 0.5^\circ\text{C}$  during 24 h to reach an equilibrium.

#### 2.1.2. CO<sub>2</sub>-measurement

After equilibration, 25 ml of the broth were taken and if necessary diluted with cooled distilled water. The pH of the mixture was adjusted with a sodium citrate buffer (pH 4) to 5.0. The concentration of CO<sub>2</sub> in the broth was immediately measured with an Orion Carbon Dioxide Electrode, model 95-02, Orion, Boston, USA. A calibration curve was prepared before every measurement with three appropriate NaHCO<sub>3</sub> standards. A correction was made

for the added buffer solution. The CO<sub>2</sub>-concentration in the broth of all bottles was measured in duplicate.

### 2.1.3. Experimental design

The experiments were designed according to the fractional factorial Box-Behnken Design (Khuri and Cornell, 1987) with five independent variables (gas/product volume ratio, initial CO<sub>2</sub>-concentration in the gas-phase, temperature, pH and lard content). A Box-Behnken design is formed by combining two-level factorial designs with balanced incomplete block designs. The different levels of the five investigated parameters are presented in Table 1. The gas/product volume ratio was defined as the ratio of the volume of gas over the volume of broth in the bottles (exclusive of the lard).

The central point was repeated 12 times in order to evaluate the repeatability of the developed method. Each other combination was performed in duplicate, resulting in a total of 92 measurements.

### 2.1.4. Statistical analysis

From the obtained data a second order response surface equation was derived by stepwise regression with a Householder factorisation algorithm by means of the software package Design Expert Software, version 5.0, Stat-Ease Inc., Minneapolis.

## 2.2. Development of a model for the amount of dissolved carbon dioxide as a function of the initial CO<sub>2</sub>-concentration, gas/product volume ratio and temperature

### 2.2.1. Experimental design

Sample preparation and CO<sub>2</sub>-measurements were performed as described in Section 2.1.1 and Section 2.1.2, respectively.

The amount of dissolved CO<sub>2</sub> was determined by means of a full factorial design of three temperatures (4°C, 8°C and 12°C), five gas/product volume ratios (0.3, 0.8, 1.3, 2.5 and 4.0) and five initial CO<sub>2</sub> gas concentrations (10%, 35%, 60%, 80%, 100% CO<sub>2</sub> compensated with N<sub>2</sub>). pH was adjusted to 6.1 and no lard was added. Each combination was performed in duplicate, resulting in a total of 150 measurements.

### 2.2.2. Statistical modeling

From the obtained data a second order response surface model was developed as described above.

A second equation was also derived based on the physical character of the CO<sub>2</sub>-dissolving process. The concentration of CO<sub>2</sub> in solution at equilibrium is normally expressed by Henry's law (Dixon and Kell, 1989):

$$(\text{CO}_2)_{\text{aq}}^E = K \cdot p\text{CO}_2 \quad (1)$$

where  $K$  = Henry's constant (g/l atm),  $p\text{CO}_2$  = partial pressure of CO<sub>2</sub> in the gas-phase at equilibrium (atm),  $(\text{CO}_2)_{\text{aq}}^E$  = concentration of CO<sub>2</sub> in the water-phase at equilibrium (g/l).

By application of the ideal gas law, partial mass balances for CO<sub>2</sub> and  $W_{\text{CO}_2} = \rho_{\text{CO}_2} / \text{Vol}_{\text{CO}_2}$  where  $W_{\text{CO}_2}$  is the weight of CO<sub>2</sub> in the gas or water-phase (g),  $\rho_{\text{CO}_2}$  is the density of CO<sub>2</sub> (g/l) and  $\text{Vol}_{\text{CO}_2}$  is the volume taken by CO<sub>2</sub> (l), the following quadratic equation is obtained:

$$\begin{aligned} & ((\text{CO}_2)_{\text{aq}}^E)^2 - \left( \frac{G}{P} \cdot \rho_{\text{CO}_2} + K \right) \cdot (\text{CO}_2)_{\text{aq}}^E \\ & + K \cdot \% \text{CO}_{2\text{g}}^I \cdot \rho_{\text{CO}_2} / 100 = 0 \end{aligned} \quad (2)$$

where  $(G/P)$  = gas/product volume ratio,  $\% \text{CO}_{2\text{g}}^I =$

Table 1

Levels of the examined parameters used in a Box-Behnken design to investigate the influence of intrinsic and extrinsic parameters on the CO<sub>2</sub>-solubility

Independent variable	Level		
	-1	0	+1
Gas/product volume ratio	0.50	2.25	4.00
Initial CO <sub>2</sub> -concentration in the gas-phase (%)	10	55	100
Temperature (°C)	4	7	10
pH	4.5	6.0	7.5
Lard fraction (v/v)	0.0	0.2	0.4

the initial CO<sub>2</sub>-concentration in the gas phase (vol.%).

From Eq. (2), the following solution is obtained:

$$(\text{CO}_2)_{\text{aq}}^E = \frac{\left(\frac{G}{P} \cdot \rho_{\text{CO}_2} + K\right) - \sqrt{\left(\left(\frac{G}{P} \cdot \rho_{\text{O}_2} + K\right)^2 - 4 \cdot K \cdot \frac{G}{P} \cdot \% \text{CO}_2^i \cdot \rho_{\text{CO}_2} / 100\right)}}{2} \quad (3)$$

### 2.3. Influence of different packaging configurations on the growth of *Pseudomonas fluorescens*

#### 2.3.1. Test organism

*Pseudomonas fluorescens* (LMG 1794) was chosen as test organism.

#### 2.3.2. Experimental set-up

To illustrate the possible use of the concentration of CO<sub>2</sub> in the water-phase of a food as a parameter for the effectiveness of a modified atmosphere, growth curves of *P. fluorescens* were measured at 7°C. For experiment 3A growth curves were determined for five different CO<sub>2</sub>-concentrations (after equilibrium) in the broth (Table 2). In experiment 3B growth curves of *P. fluorescens* were determined at three different combinations of initial CO<sub>2</sub>-concentration and G/P volume ratio (Table 2). All the combinations of experiment 3B resulted in a final CO<sub>2</sub>-concentration of 800 ppm in the broth. A jar filled with modified BHI (gas/product volume ratio=1.5) and gas packed under 80% N<sub>2</sub>/20% O<sub>2</sub> was functioning as a blank. All growth curves were determined in duplicate.

*P. fluorescens* was subcultured in APT-broth (BBL, 10918) for 24 h at 30°C. A second subculture was incubated in APT-broth for 16 h at 30°C and was placed for 6 h at 7°C before inoculation, to allow the test strain to adapt to the chilling temperature. After the adaptation period, the modified BHI-broth in the jars (see Section 2.1.1) was inoculated to a level of  $\pm 10^4$ /ml.

After inoculation, the jars were immediately gas packed as described in Section 2.1.1 and stored at 7°C. At regular time intervals, samples (0.2 ml) were taken with a sterile disposable 1-ml syringe, diluted if necessary with Peptone Physiological Salt solution (0.1% peptone, 0.85% NaCl) and plated in duplicate on Plate Count Agar (Oxoid, CM325) with a Spiral Plater Model D (Spiral Systems Inc., Cincinnati, USA). The plates were aerobically incubated during 3 days at 30°C before counting.

## 3. Results and discussion

### 3.1. Screening for the importance of intrinsic and extrinsic factors on the CO<sub>2</sub>-solubility

Fig. 1 represents the perturbation plot for the effect of the investigated parameters on the amount of CO<sub>2</sub> which is dissolved in modified BHI. In a perturbation plot, the response (here the amount of dissolved CO<sub>2</sub> (ppm)) is plotted by changing only one factor over its range while holding all other factors constant at the central level.

The amount of CO<sub>2</sub> dissolved in the broth was shown to be mainly affected by two factors: the

Table 2  
Different applied packaging configurations resulting in a specific target concentration of dissolved CO<sub>2</sub>

Experiment no.	Target dissolved CO <sub>2</sub> (ppm)	Packaging configuration			
		O <sub>2</sub> (%)	N <sub>2</sub> (%)	CO <sub>2</sub> (%)	Gas/product (ml/ml)
3A	0	20.0	80.0	0.0	1.50
	500	20.0	56.0	24.0	1.50
	1000	20.0	20.0	60.0	1.50
	1500	20.0	16.0	64.0	3.40
	2000	14.0	10.0	86.0	4.00
3B	0	20.0	80.0	0.0	1.50
	800	20.0	20.0	60.0	0.97
	800	20.0	39.8	40.2	1.74
	800	20.0	48.6	31.4	4.00

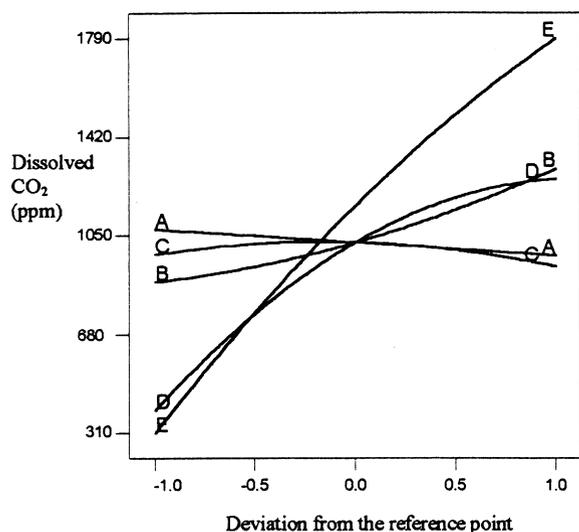


Fig. 1. Perturbation plot for the effect of the fat/product volume fraction (A), pH (B), temperature ( $^{\circ}\text{C}$ ) (C), gas/product volume ratio (D) and the initial  $\text{CO}_2$ -concentration in the head space (%) (E) on the amount of  $\text{CO}_2$  dissolved in modified BHI (ppm).

initial  $\text{CO}_2$ -concentration in the gas-phase and the gas/product volume ratio. Temperature was shown to influence the solubility of  $\text{CO}_2$  only slightly in the applied temperature range ( $4\text{--}12^{\circ}\text{C}$ ) and in comparison with the effect of the other investigated parameters. The effect of temperature, initial  $\text{CO}_2$ -concentration and gas/product volume ratio will be further discussed in Section 3.2.

Fig. 1 also illustrates the significant effect of pH on the  $\text{CO}_2$ -solubility. An increase in pH resulted in an increase of the  $\text{CO}_2$ -solubility and this effect was strongest at high pH values. Similar results were demonstrated by Löwenadler and Rönner (1994). This can be explained by the equilibrium reactions which occur when  $\text{CO}_2$  dissolves in the food. At the moment  $\text{CO}_2$  is dissolved, it will be hydrated and carbonic acid will be formed.

This will be dissociated to form a bicarbonate ion and a hydrogen ion. At low pH (read high  $\text{H}^+$ -concentrations) the reaction will be pushed towards the direction of  $\text{CO}_2$  and consequently lower amounts of  $\text{CO}_2$  will be able to dissolve in the water-phase.

When  $\text{CO}_2$  dissolves in the fat-phase of a food, part of the  $\text{CO}_2$  in the gas-phase will be consumed and thus less will be left to dissolve in the water-phase of the food which results in a lower  $\text{CO}_2$ -

concentration in the water-phase in fatty foods. It is generally known that products with a high fat content (salads, fatty fish, ...) very often show collapsing because of the  $\text{CO}_2$  dissolving in the fat-phase. The fat-phase of the above mentioned products mainly consists of unsaturated oils. Fig. 1 shows that the lard content did not strongly influence the amount of  $\text{CO}_2$  dissolved in the water-phase. The low solubility of  $\text{CO}_2$  in the lard can possibly be explained by the high solid fat index of lard at the applied low temperatures.

### 3.2. Development of a model for the amount of dissolved carbon dioxide as function of the initial $\text{CO}_2$ -concentration, gas/product volume ratio and temperature

The coefficients, the square root of the mean square error and the adjusted  $R^2$  for the quadratic response equation for the amount of dissolved  $\text{CO}_2$  as function of the gas/product ratio ( $G/P$ ), the initial  $\text{CO}_2$ -concentration in the gas phase (%) and the temperature are given in Table 3. In Fig. 2 the observed values for the dissolved  $\text{CO}_2$  are plotted against the values predicted by the developed response surface model without modification of the response. The observed values were close to the predicted values which demonstrates, in combination with the high adjusted  $R^2$ , the usefulness of the model to predict the amount of dissolved  $\text{CO}_2$  in

Table 3

Unscaled coefficients of the quadratic response surface equation for the amount of carbon dioxide dissolved as a function of the gas/product volume ratio, the initial  $\text{CO}_2$  gas concentration and the temperature

Parameters	Coefficient	Prob >  t
Intercept	-249.37	
Gas/product ( $G/P$ )	342.42	<0.0001
Initial % $\text{CO}_2$	14.11	<0.0001
Temperature ( $T$ )	7.1	<0.0001
$(G/P)^2$	-63.44	<0.0001
(Initial % $\text{CO}_2$ ) <sup>2</sup>	-0.045	<0.0001
$G/P \times \text{initial \%CO}_2$	3.85	0.0137
$G/P \times T$	-5.49	<0.0001
Initial % $\text{CO}_2 \times T$	-0.35	<0.0001
RMSE	87.1	
Adjusted $R^2$	0.9801	

RMSE, square root of the mean square error.

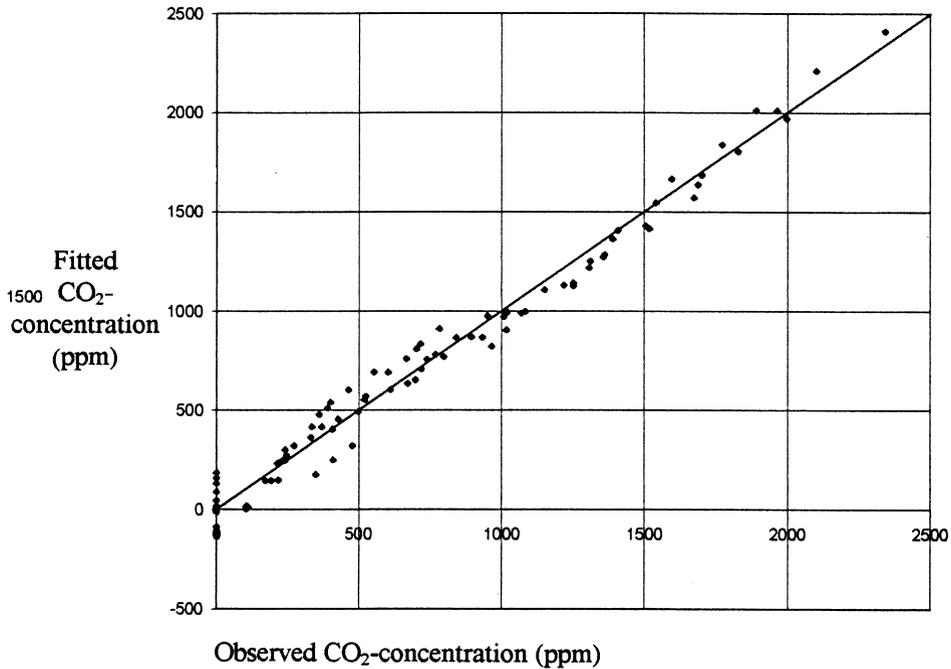


Fig. 2. Observed versus fitted values of the developed model for the dissolved  $\text{CO}_2$  as a function of temperature, gas/product volume ratio and initial  $\text{CO}_2$ -concentration.

modified BHI-broth as a function of the investigated parameters.

When the data at the different experimental temperatures were separately fitted towards Eq. (3), good correlation was obtained. The derived Henry constants  $K$  and the corresponding correlation coefficients for the different temperatures are presented in Table 4. Eq. (3) shows how to describe the amount of dissolved carbon dioxide as a function of the initial  $\text{CO}_2$  gas concentration and the gas/product volume ratio. When Eq. (3) will be used in practice, Henry constants of the packed product will have to be determined. These Henry constants are dependent on temperature and the type of food ( $a_w$ , pH, water content, buffer capacity, ...). Eq. (3) can be a powerful tool in the quantification of the effect

of different intrinsic and extrinsic parameters on the solubility of  $\text{CO}_2$  in food products. For further discussion however, the response surface equation will be used because of the inclusion of temperature as an independent variable.

Fig. 3 represents the contour plots of the response surface equation for the amount of  $\text{CO}_2$  (ppm) dissolved in modified BHI-broth as a function of the initial  $\text{CO}_2$ -concentration (%) in the gas-phase, the gas/product volume ratio (A) and the temperature (B). The initial  $\text{CO}_2$ -concentration in the gas-phase was shown to have a strong influence on the amount of dissolved  $\text{CO}_2$  in the water-phase, as also reported by Löwenadler and Rönner (1994). More remarkable however was the significant effect of the gas/product volume ratio ( $G/P$ ) on the amount of  $\text{CO}_2$  which

Table 4  
Henry's constants  $K$  and correlation coefficients  $R^2$  for Eq. (3) at the different experimental temperatures

Temperature (°C)	$K$	95% lower confidence interval value	95% upper confidence interval value	$R^2$
4	2.841	2.583	3.098	0.950
8	2.541	2.331	2.751	0.956
12	2.223	2.030	2.417	0.948

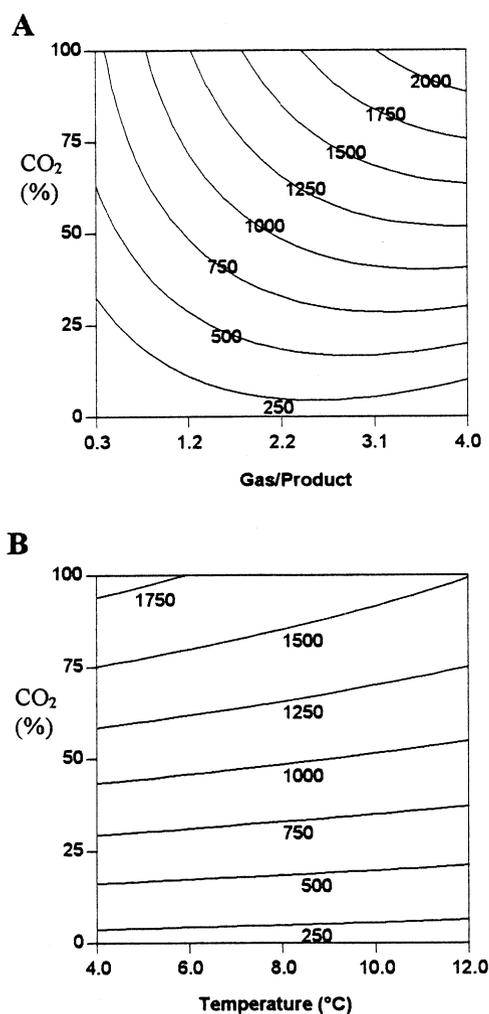


Fig. 3. Contour plots of the amount of carbon dioxide (ppm) dissolved in modified BHI-broth as a function of the initial  $\text{CO}_2$ -concentration in the gas phase (%), gas/product volume ratio (A) and temperature ( $^{\circ}\text{C}$ ) (B).

was dissolved in the broth. An increase of the  $G/P$  from 0.3 to 2.0 (at  $8^{\circ}\text{C}$  and initial  $\text{CO}_2$ -concentration in the gas-phase = 50%), resulted in an increase of the amount of  $\text{CO}_2$  dissolved in the modified BHI-broth of 145% (402 ppm to 989 ppm). For all  $\text{CO}_2$ -concentrations, the influence of the  $G/P$  was highest at low  $G/P$  ratios. This can be explained by the larger drop of the  $\text{CO}_2$  concentration with the gas-phase in case of low  $G/P$  ratios when  $\text{CO}_2$  starts dissolving.

At equilibrium, this will result in a low residual

$\text{CO}_2$ -concentration in the gas-phase and thus a low amount of  $\text{CO}_2$  dissolved in the water phase. This illustrates clearly the importance of the optimisation of a packaging configuration of a modified atmosphere package. Moreover, the importance of the gas/product volume ratio on the amount of  $\text{CO}_2$  which will dissolve in the water-phase of a food demonstrates the incompatibility of the diverse published data concerning MAP. Data without mentioning the applied gas/product volume ratio and the moisture content of the product will be difficult to compare.

Temperature was shown to influence only slightly the amount of dissolved  $\text{CO}_2$  compared to the other investigated parameters (Fig. 2B). When the temperature was increased from 4 to  $12^{\circ}\text{C}$  ( $G/P=2$ , initial  $\text{CO}_2$ -concentration in the gas-phase = 50%), a decrease in the solubility of  $\text{CO}_2$  of 16% (1073 ppm to 901 ppm) was noticed. This is comparable with the results of Löwenadler and Rönner (1994) and Lange (1956), who reported a decrease of, respectively, 17.1% and 22.8% (in nutrient broth and water, respectively) when temperature was increased from 4 to  $12^{\circ}\text{C}$ . Although the minor effect of modified atmospheres at higher temperatures has been attributed by many authors to the lower solubility of carbon dioxide (Wolfe, 1980; Wimpfheimer et al., 1990; Zhao et al., 1994), the present results demonstrate only a minor effect of the temperature on the  $\text{CO}_2$ -solubility at a realistic chilling temperature range ( $4$ – $12^{\circ}\text{C}$ ). This demonstrates that the high effect of  $\text{CO}_2$  at low temperatures will not only be attributed to the higher solubility of  $\text{CO}_2$  but also to a higher sensitivity of the microbial cell for  $\text{CO}_2$  at low temperatures. Further investigations are however necessary to prove this statement.

### 3.3. Influence of different packaging configurations on the growth of *Pseudomonas fluorescens*

The growth of *P. fluorescens* was highly influenced by  $\text{CO}_2$  as shown in Fig. 4. A significant increase in the lag phase and decrease in the growth rate of *P. fluorescens* was, as could be expected, noticed with increasing  $\text{CO}_2$ -concentrations. A more remarkable result is however shown in Fig. 5. The growth characteristics of *P. fluorescens* in the three packaging configurations resulting in 800 ppm of  $\text{CO}_2$  in the medium, showed no significant differ-

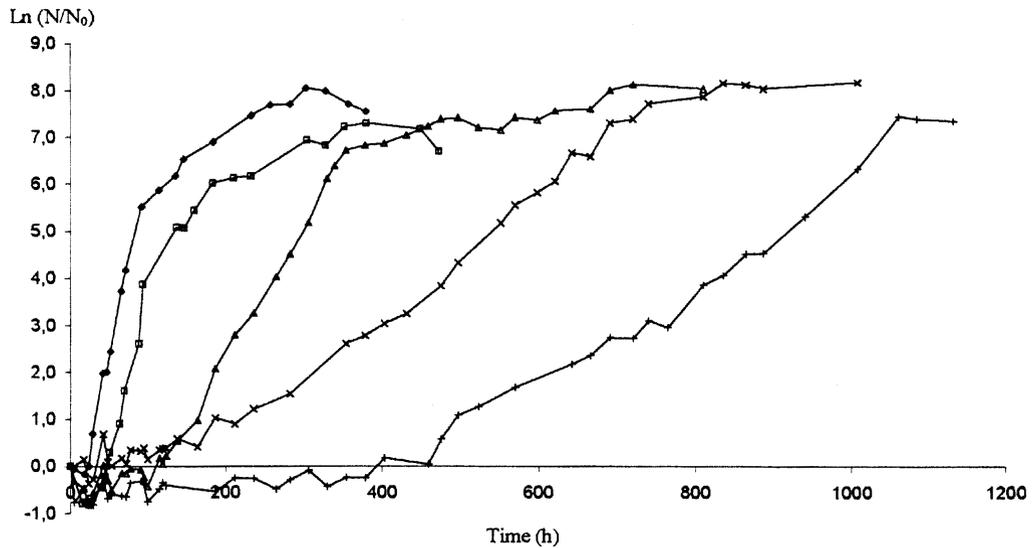


Fig. 4. Influence of CO<sub>2</sub> on the growth of *P. fluorescens* at 7°C for different CO<sub>2</sub>-concentrations (◇ 0 ppm, □ 500 ppm, △ 1000 ppm, × 1500 ppm and + 2000 ppm) in modified BHI-broth (experiment 3A).

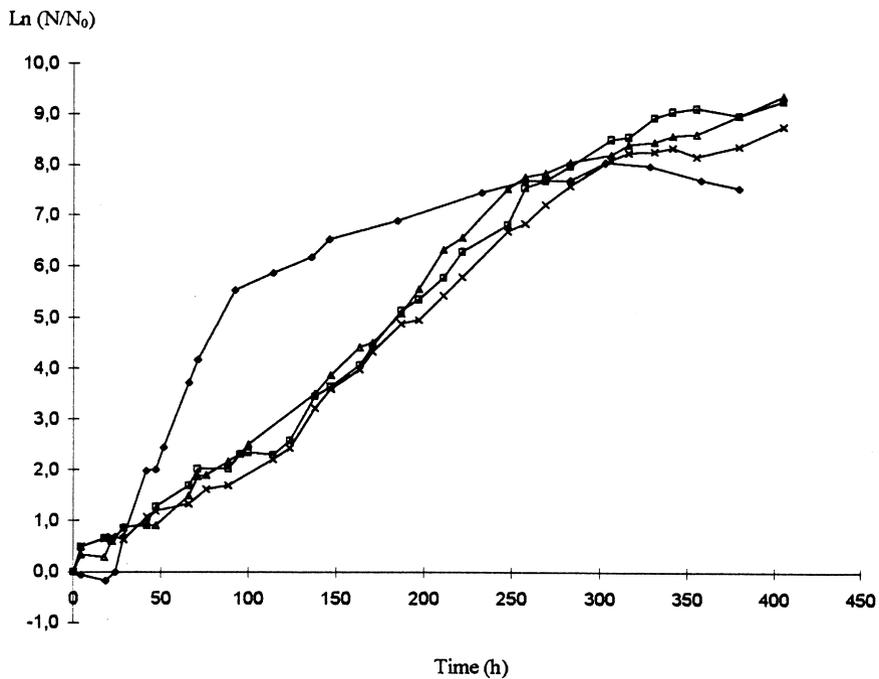


Fig. 5. Influence of CO<sub>2</sub> on the growth of *P. fluorescens* at 7°C for different packaging configurations (◇ 0% CO<sub>2</sub> — 1.5 G/P, □ 31.4% CO<sub>2</sub> — 4.0 G/P, △ 40.2% CO<sub>2</sub> — 1.74 G/P, × 60% CO<sub>2</sub> — 0.97 G/P), resulting in 800 ppm of CO<sub>2</sub> in modified BHI-broth (experiment 3B).

ences at 7°C. The three configurations resulted in the same inhibition rate of *P. fluorescens* compared to the growth in the packaging configuration without CO<sub>2</sub>. The three packaging configurations differed strongly in initial gas composition. This proves the statement that CO<sub>2</sub> exerts its antimicrobial effect in the water-phase of a food product. The combination of the results of Figs. 4 and 5 illustrates the usefulness of the dissolved CO<sub>2</sub> in the water-phase of a food product to define a modified atmosphere packaging system regarding its antimicrobial effect. Optimisation of modified atmosphere packaging should be based on a maximisation of the amount of CO<sub>2</sub> dissolved in the water-phase of the specific food product. During this process, the antimicrobial effects will however always be confronted with sensorial and marketing aspects which will at the end result in an optimal product. The initial CO<sub>2</sub>-concentration is however mostly used as the only parameter to characterise a modified atmosphere packaging configuration. When the effect of modified atmospheres on the microbial spoilage or safety of food products is modeled, the CO<sub>2</sub> dissolved in the water-phase of the food should be incorporated in the model as an independent variable (Devlieghere et al., 1998).

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